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S P E C I F I C A T I O N

2 A RADIAL DISPERSION MASS TRANSFER DEVICE  
3 HAVING A SEMI-PERMEABLE TUBULAR HOLLOW FIBER  
4 MEMBRANE WOUND AROUND A POROUS CORE

## 5 BACKGROUND OF THE INVENTION

6 The field of the invention is mass transfer devices and the  
7 invention relates more particularly to devices that are  
8 constructed to pass a bulk fluid along the exterior surface of a  
9 plurality of hollow fibers. One such device is shown in U.S.  
10 Patent No. 3,794,468. A porous cylindrical core is wound with a  
11 single length of capillary tubing as the core is being turned. A  
12 core insert directs the bulk fluid from the interior of the  
13 porous core over the exterior of the capillary tubes and out of  
14 the outlet tubes. A second fluid passes counter currently  
15 through the interior of the capillary tubes.

16 Another process for making a fiber bundle is shown in U.S.  
17 Patent No. 4,572,446. Again, a bundle of hollow fibers are wound  
18 around a length of a core.

19 A similar design is shown in U.S. Patent No. 5,299,749.  
20 Continuous lengths of filament are laid down on a core around a  
21 length of a core.

22 The flow of fluid within the hollow fibers and the fluid  
23 flowing on the outside of the hollow fibers is almost counter

1 current. For some separation processes, it is beneficial that  
2 the flow be more across the axis of the hollow fiber rather than  
3 along the axis of the hollow fiber.  
4

#### 5 BRIEF SUMMARY OF THE INVENTION

6 The present invention is for a mass transfer device having a  
7 fluid permeable core for the passage of a bulk fluid. The core  
8 has a bulk fluid inlet end and a bulk fluid outlet end. The core  
9 is surrounded by a bundle of hollow fibers. The core is  
10 fabricated from a sintered plastic or metal material having pores  
11 ranging in porosity from about 50 microns to about 200 microns.  
12 A baffle is positioned within the hollow center of the core so  
13 that fluid pumped into the inlet end of the core must pass  
14 outwardly through the walls of the core to get around the baffle.  
15 The fiber bundle is surrounded by a housing which forces the bulk  
16 fluid back into the side walls of the core downstream of the  
17 baffle. The fiber bundle is made from a first and a second  
18 plurality of semi permeable hollow fibers wound around the  
19 exterior of the core so that the first and second plurality of  
20 fibers form an angle between 20 and 60 degrees and preferably  
21 about 35 degrees with respect to one another.

#### 22 BRIEF DESCRIPTION OF THE SEVERAL VIEWS OF THE DRAWING

23 Figure 1 is a cross-sectional view of the mass transfer  
24 device of the present invention.

1           Figure 2 is a side view with the facing side of the housing  
2 removed from the mass transfer device of Figure 1.

3           Figure 3 is an enlarged diagrammatical view taken along line  
4 3-3 of Figure 2.

5           Figure 4 is a side view showing the winding of hollow fibers  
6 around a core in the production of the mass transfer device of  
7 Figure 1.

8           Figure 5 is a view analogous to Figure 4, but showing  
9 additional winding.

10          Figure 6 is a diagrammatical view of the mass transfer  
11 device of Figure 1 affixed to input and output streams.

#### 12                   DETAILED DESCRIPTION OF THE INVENTION

13          The mass transfer device of the present invention is  
14 indicated in cross-sectional view in Figure 1 by reference  
15 character 10. Device 10 has a fluid permeable core 11. Hollow  
16 fiber bundle 12 is wrapped around exterior surface 13 of core 11.  
17 Core 11 has an inner surface 14 which surrounds an inner  
18 passageway 15. Permeable core 11 is in two halves and is joined  
19 by the ends of baffle 16. Baffle 16 is sealed to bore 11 by O-  
20 rings 16'.

21          A baffle 16 blocks the flow of fluid in inner passageway 15.  
22 Thus, bulk fluid entering the device, as indicated by reference  
23 character 17 through bulk fluid inlet fitting 17', must pass  
24 through the side walls of core 11, as indicated by arrows 17.

1 Core 11 has a bulk fluid inlet end 32 and a bulk fluid outlet end  
2 33. The fluid flow path 17 passes completely through fiber  
3 bundle 12 to an outer gap 12' between the outer edge of the  
4 bundle 12 and the inner surface of housing 20.

5 The details of the fluid passageway around the exterior of  
6 hollow fiber bundle 12 is shown best in Figure 3 and discussed  
7 below. Broadly, however, bulk fluid passes back into interior  
8 passageway 15, as indicated by arrows 18, and leaves through bulk  
9 fluid outlet fitting 19.

10 Hollow fiber bundle 12 is surrounded by housing 20 which has  
11 a housing inlet end 21 and a housing outlet end 22.

12 Hollow fiber bundle 12 is subjected to the flow of bulk  
13 fluid around the exterior surfaces of the individual hollow  
14 fibers. A bore fluid flows through the interior of the hollow  
15 fiber bundle. This is accomplished by potting the ends of the  
16 bundle in a curable sealant 23 at a bore fluid exit end 24.  
17 Similarly, a curable sealant 25 is sealed around the bore fluid  
18 entrance end 26. A bore fluid exit manifold 27 surrounds the  
19 exterior open ends of the hollow fibers and a bore fluid entrance  
20 manifold 28 surrounds the open ends of the hollow fiber bundle  
21 12. Thus, bore fluid enters the device through bore fluid  
22 entrance fitting 29 and exits the device through bore fluid exit  
23 fitting 30. The device and the core have a longitudinal axis  
24 indicated by reference character 31.

1           The mass transfer device 10 is shown in side view in Figure  
2           2 with the housing 20 cut away. Two sets of hollow fibers 32 and  
3           33, one upwardly wound and one downwardly wound, are shown spaced  
4           apart a distance about equal to the width of one set. These are  
5           also indicated in Figure 4 in an initial winding step discussed  
6           below.

7           An enlarged view of a portion of the fiber indicated by  
8           arrow 3 in Figure 2 is shown in Figure 3. In Figure 3 the bulk  
9           fluid N is indicated by the shaded arrows 17. The bulk fluid  
10          passes into inner passageway 15. The bulk fluid 17 then passes  
11          outwardly through the side walls of the sintered fluid permeable  
12          core 11. It then passes across the outer surface of the hollow  
13          fiber bundle 12. This is shown in enlarged view in Figure 3  
14          where a hollow fiber is indicated by reference character 35. It  
15          then, having been forced around baffle 16, passes through the  
16          side walls of fluid permeable core 11 and continues to the bulk  
17          fluid outlet fitting 19. As can be seen in Figure 3, the fluid  
18          tends to flow across the outer surface of the hollow fibers 35  
19          more than it flows along parallel to the outer surfaces as  
20          generally taught by the prior art. It is believed that this  
21          provides a further anti-fouling scrubbing action of the bulk  
22          fluid against the outer surface of the fibers and helps the flow  
23          of a portion of bore fluid 34 through the walls of hollow fibers  
24          35 and into the bulk fluid.

1           The winding process of the present invention is indicated in  
2 Figure 4 where fiber feeding shuttle 36 can guide from 1 to 16  
3 individual hollow fibers 35 in a set 37 of hollow fibers. Set 37  
4 has a width 38. Each set 37 is spaced from an adjacent set by a  
5 space 39 which is preferably about equal to the width of a set.  
6 The set indicated in Figure 4 is wound at an angle "a" to the  
7 longitudinal axis 31 of core 11. Then the winding process is  
8 reversed and a second set of hollow fibers is wound as indicated  
9 in Figure 5. The second set is wound at an angle indicated by  
10 reference character b in Figure 5. Angles a & b are arranged so  
11 that the angle between the set indicated by reference character  
12 37 and the set indicated by reference character 40 are at an  
13 angle of about 35 degrees indicated by reference character "c".  
14 This angle can range between 20 and 60 degrees, but keeping this  
15 angle well below 180 degrees provides a crossflow rather than a  
16 longitudinal/tangential flow of the fluid passing within the  
17 hollow fibers and the bulk fluid passing over the exterior of  
18 the hollow fibers.

19           A schematic view of a laboratory setup is shown in Figure 6.  
20 A bulk fluid container 41 contains bulk fluid 42. This is passed  
21 through pump 43, pressure gauge 44, and into bulk fluid entrance  
22 fitting 17'. It passes upwardly through the mass transfer device  
23 10 and out of bulk fluid exit fitting 19. While the bulk of the  
24 above discussion has indicated counter-current flow, the diagram  
25 of Figure 6 depicts co-current flow. Thus, the bore fluid passes

1       into inlet fitting 29 through the center of the hollow bores and  
2       hollow fibers 35 and out the bore fluid outlet fitting 30. The  
3       bore fluid is indicated by reference character 45.

4             The present embodiments of this invention are thus to be  
5       considered in all respects as illustrative and not restrictive;  
6       the scope of the invention being indicated by the appended claims  
7       rather than by the foregoing description. All changes which come  
8       within the meaning and range of equivalency of the claims are  
9       intended to be embraced therein.